

# Optimization Problems in Gas Transportation

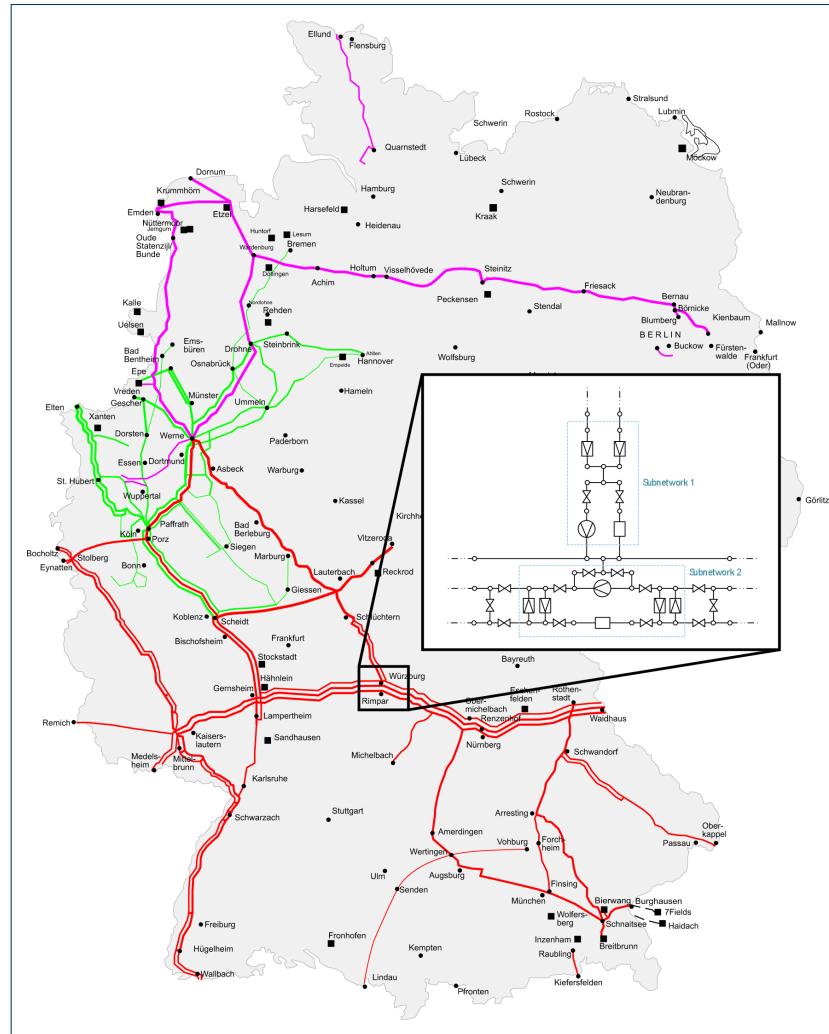
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CWM<sup>3</sup>EO 2014, Budapest

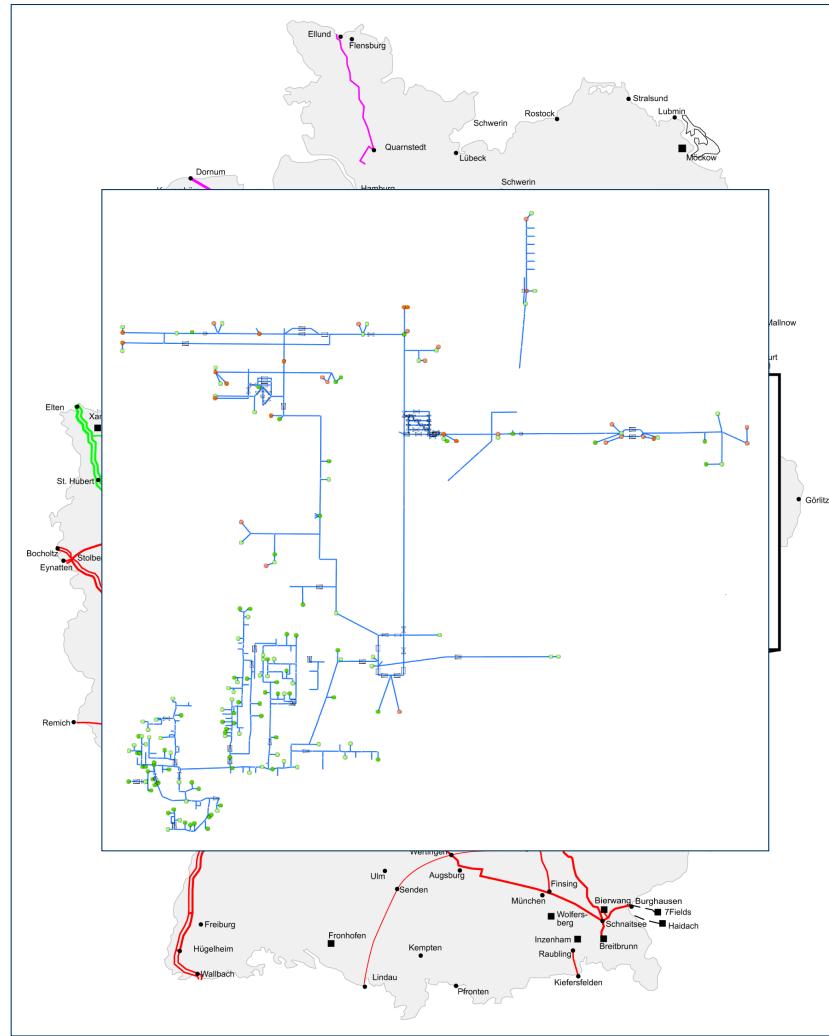


WIRTSCHAFTS  
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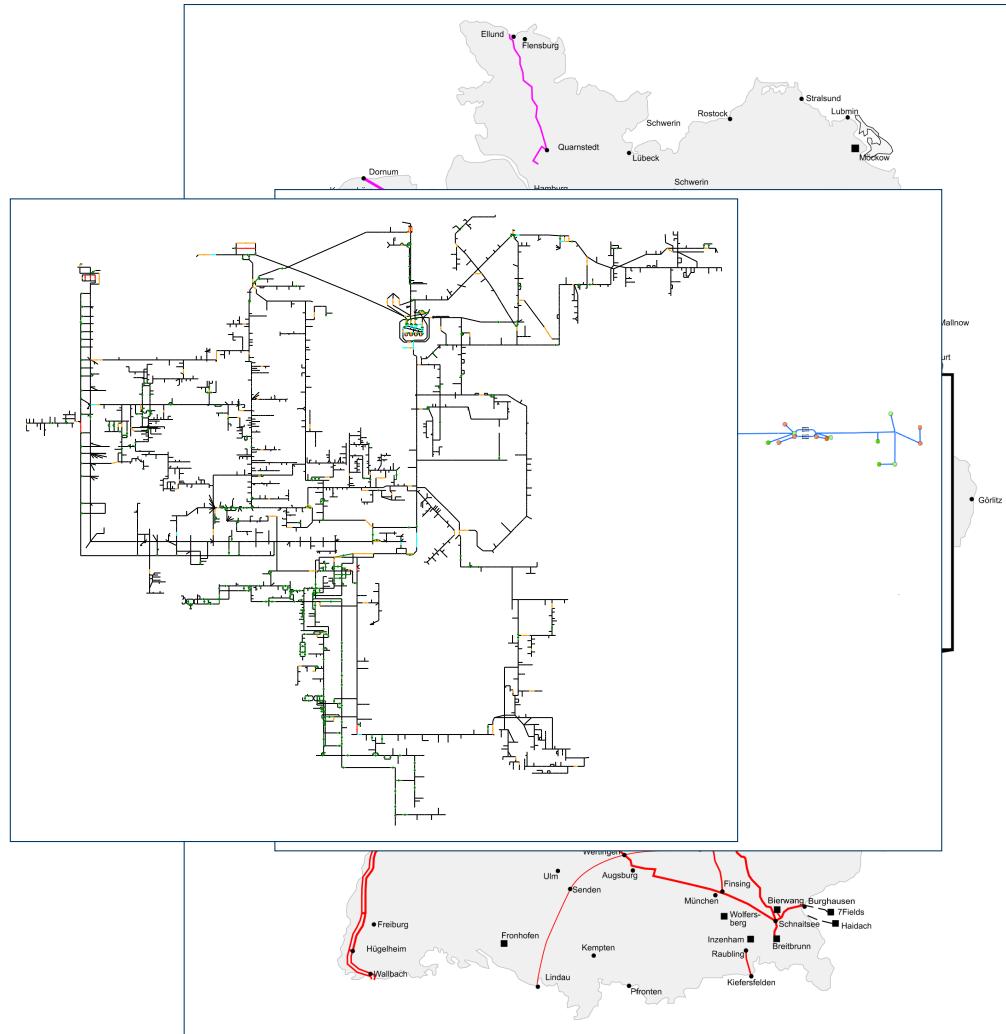
# Why do we care?



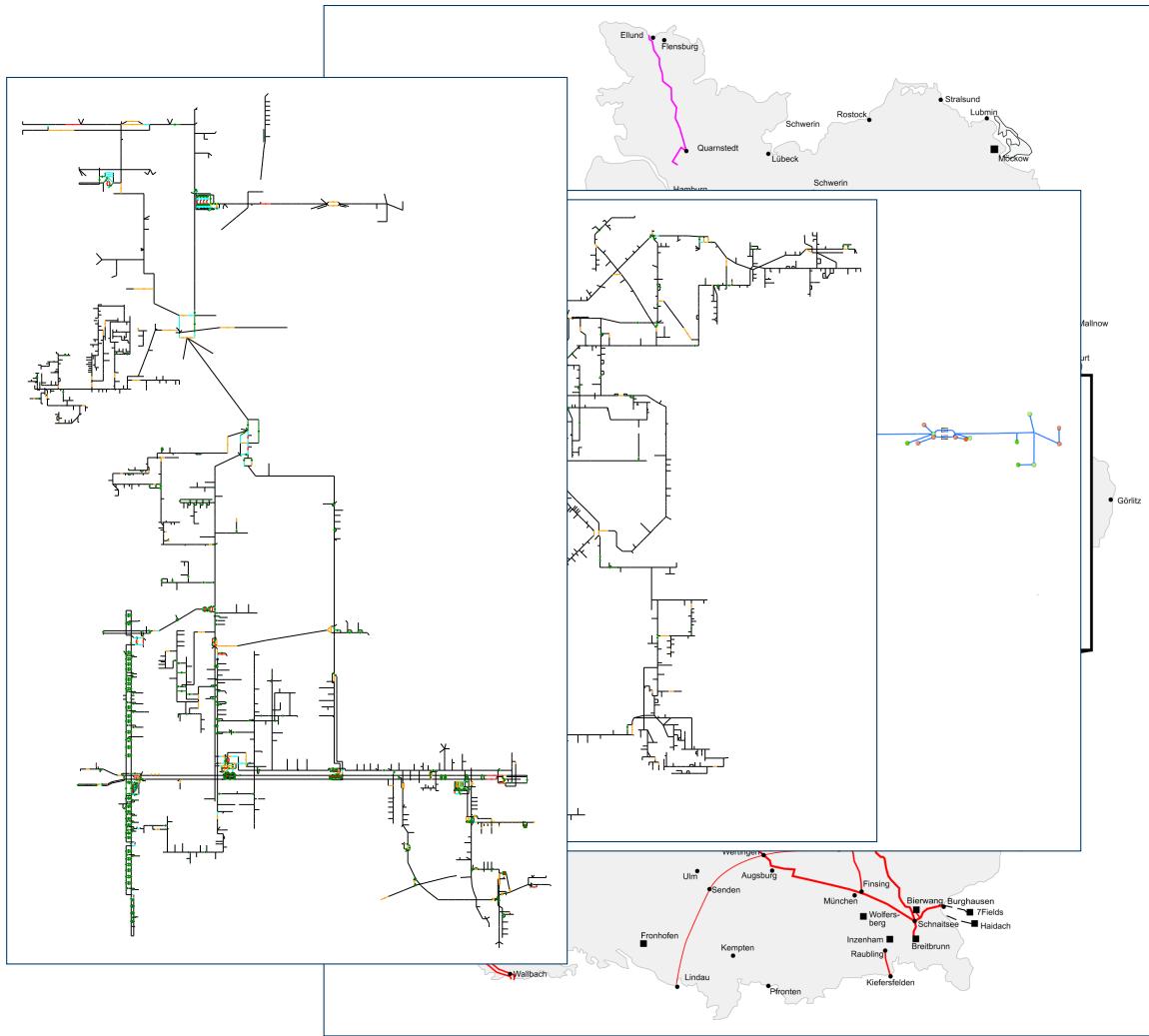
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# Why do we care?

## Interesting MINLP

- Lots of structure,
- challenging nonlinearities,
- many problem variants.

## Infeasibility important . . .

- needed to certify rejections

## Good setting to test MINLP methods

## Advertisement: Our book

# Evaluating Gas Network Capacities

Koch, Hiller, Pfetsch, Schewe (Eds.),  
to appear in the SIAM-MOS series, December 2014

# Structure of the Project

## Funding

- Open Grid Europe
- German Federal Government

## Partners

- FAU Erlangen-Nuremberg
- Humboldt University Berlin
- Leibniz University Hannover
- TU Braunschweig
- University Duisburg-Essen
- Weierstraß Institute Berlin
- Zuse Institute Berlin

# What are the problems?

# Problems

## Standard contract

*“On any given day you are allowed to supply/demand up to  $X$  units of gas at node  $v$  if you have matching partners at some other nodes”*

## Problems

- Given a supply/demand situation on a given day, is it technically feasible?
- How large may  $X$  be?
- Given a set of nodes, how large may we choose each  $X_v$  such they can be satisfied simultaneously?
- If one of the above problems has no satisfying solution, where can we build a network extension to ameliorate the situation?

# Validation of nominations – Prerequisites

## Given

- (stationary) gas network  
complete specification of all pipes, compressors, valves, ...
- active elements: compressors, valves, control valves, resistors
- temperature

## Nomination

- Precise supply amounts at entry nodes
- Precise demands at exit nodes
- Pressure bounds at entries/exits
- Balance: flow in = flow out

# Validation of nominations – Task

## Given

- a specification of the network,
- a nomination, defining supplies/demands.

## Task: Find

1. Settings for active elements  
(valves, control valves, compressors) and
2. values for physical network parameters,  
which satisfy
  - laws of physics (according to the model) and
  - regulatory and technical requirements.

# Booking validation

Given a new contract at node  $u$ , how large may we choose  $X_u$ , such that all supply/demand-scenarios can be satisfied?

- Is *not* a robust optimization problem,
- how to deal with the infinite scenario space?

# Calculation of technical capacities in gas networks?

Given a set of nodes, how large may we choose each  $X_v$ , such that all supply/demand-scenarios can be satisfied?

Definition according to GasNZV

*Technical capacity is the maximal fixed capacity which the network operator can offer guaranteeing system integrity and fulfilling all restrictions of network operation.*

# Problem: Capacity maximization

## Goal

Tool to compute available technical capacity

## Problem

Given:

- a technical specification of the gas network
- technical and contractual requirements

Find:

- *maximal* capacity,
- such that *all* (conforming) nominations can be transported.

# Validation of nominations: Physical modeling

# Modeling – Discrete and Nonlinear

## Nonlinear

- Pipes
- Compressors
- Resistors

## Discrete

- Valves
- “Control Valves”
- Switching inside compressor stations

# Network model

## Basic model

Graph  $G$  with node set  $V$  and arc set  $A$

## Nodes

- Entries, exits, and inner nodes

## Arcs

- Pipes, Resistors, ...

## Quantities

- pressure  $p$ , mass flow  $q$ ,
- density  $\rho$ , and temperature  $T$

# Hierarchical modeling

There is no true model

- need approximations,
- which typically come in hierarchies.

Are your solutions truly feasible?

- For which model?
- Does this translate to other models?
- Can you detect infeasibility?

# Pipes

## 1d Euler equations for cylindrical pipes

$$\frac{\partial \rho}{\partial t} + \frac{1}{A} \frac{\partial q}{\partial x} = 0, \quad (\text{continuity})$$

$$\frac{1}{A} \frac{\partial q}{\partial t} + \frac{\partial p}{\partial x} + \frac{1}{A} \frac{\partial(q v)}{\partial x} + g \rho s + \lambda(q) \frac{|v| v}{2D} \rho = 0, \quad (\text{momentum})$$

$$A \rho c_p \left( \frac{\partial T}{\partial t} + v \frac{\partial T}{\partial x} \right) - A \left( 1 + \frac{T}{z} \frac{\partial z}{\partial T} \right) \frac{\partial p}{\partial t} -$$

$$A v \frac{T}{z} \frac{\partial z}{\partial T} \frac{\partial p}{\partial x} + A \rho v g s + \pi D c_{HT} (T - T_{soil}) = 0,$$

needed additionally

$$\rho R_s T z(p, T) = p. \quad (\text{state})$$

# Plus ...

## Model for the real gas factor $z$

**AGA-8**  $z(p, T) = 1 + 0.257 p_r - 0.533 p_r / T_r,$

**Papay**  $z(p, T) = 1 - 3.52 p/p_c e^{-2.26 T/T_c} + 0.247 (p/p_c)^2 e^{-1.878 T/T_c},$

or ...

## Model for the friction coefficient $\lambda$

**Hagen-Poiseuille (laminar)**  $\lambda(q) = \frac{64}{Re(q)},$

**Prandtl-Colebrook (turb.)**  $\frac{1}{\sqrt{\lambda}} = -2 \log_{10} \left( \frac{2.51}{Re(q) \sqrt{\lambda}} + \frac{k}{3.71 D} \right),$

or ...

# For our model: only stationary and isothermal . . .

After simplification: System can be solved!

$$p_v^2 = \left( p_u^2 - \Lambda |q| q \frac{e^S - 1}{S} \right) e^{-S}$$



$\Lambda$  calculated from gas- and pipe-parameters

$S$  calculated from the height difference of the nodes

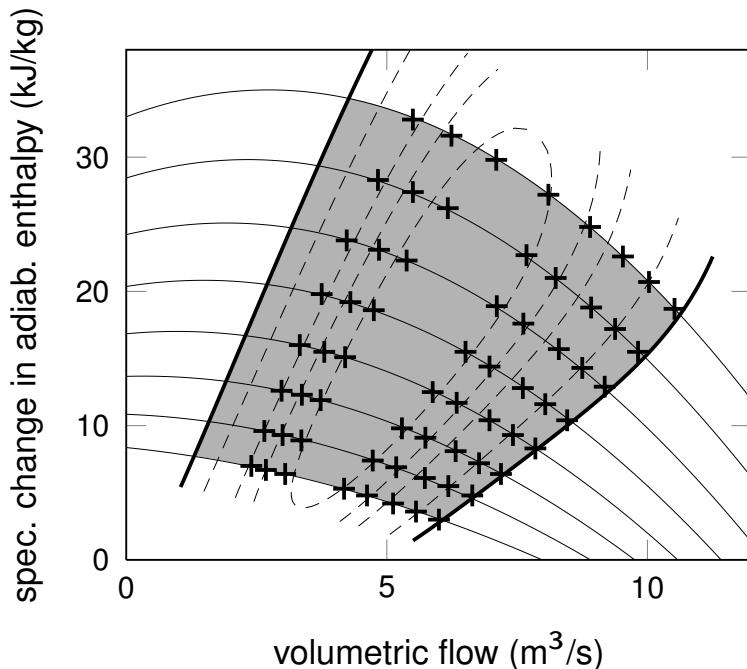
# More precisely . . .

$$\tilde{S} := \frac{2gs}{R_s z_m T_m}, \quad \tilde{\lambda} := \lambda(q) \frac{R_s z_m T_m}{A^2 D}.$$

## Parameter uncertainties

Many of these parameters are only rough approximations

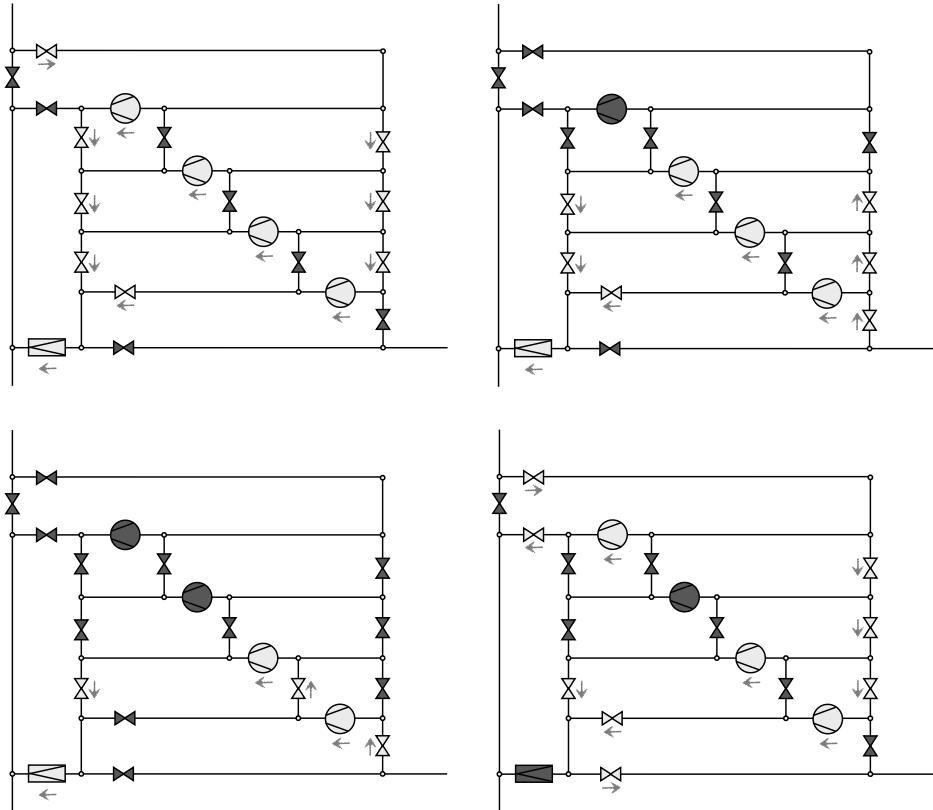
# Compressors



Modeled by

- Characteristic diagrams
- Highly nonlinear,
- no underlying PDE model.

# Subnetwork Operation Modes



- Discrete Decisions cannot be taken independently,
- only reduced set allowed for each compressor station.

# Mathematical approaches to validate nominations

# Easy cases

Much is known about ...

- Pure pipe networks,
- easy graphs, like paths and trees.

Methods

- Pure pipe networks: Can be transformed to a convex problem,
- Easy graphs: Dynamic Programming (see the survey by Carter).

# What did we do?

## Two stage approach

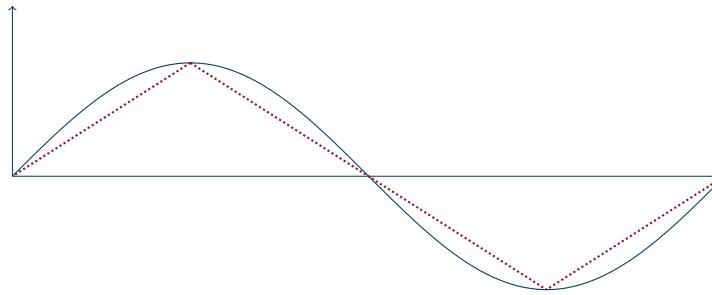
- First stage tries to compute discrete decisions (coarse models),
- Second stage checks these decisions (fine NLP model).

## First stage

- Exact:
  - MILP-relaxation,
  - “special” MINLP-approach,
- Heuristic:
  - MPEC,
  - “reduced” NLP-approach + assignment heuristic.

# Basis of our approach

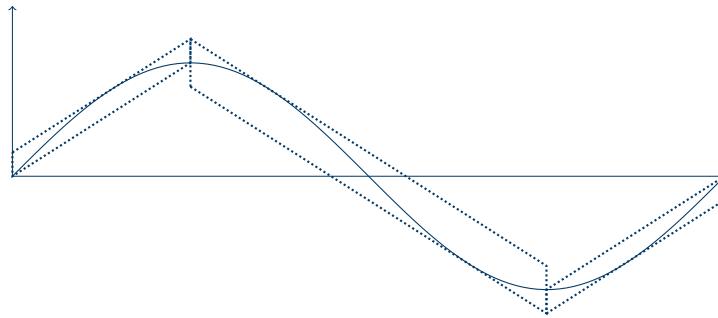
Classical: MIP approximations



- uses MIP formulations to approximate nonlinear constraints, e.g. incremental method or convex combination method.

# Basis of our approach

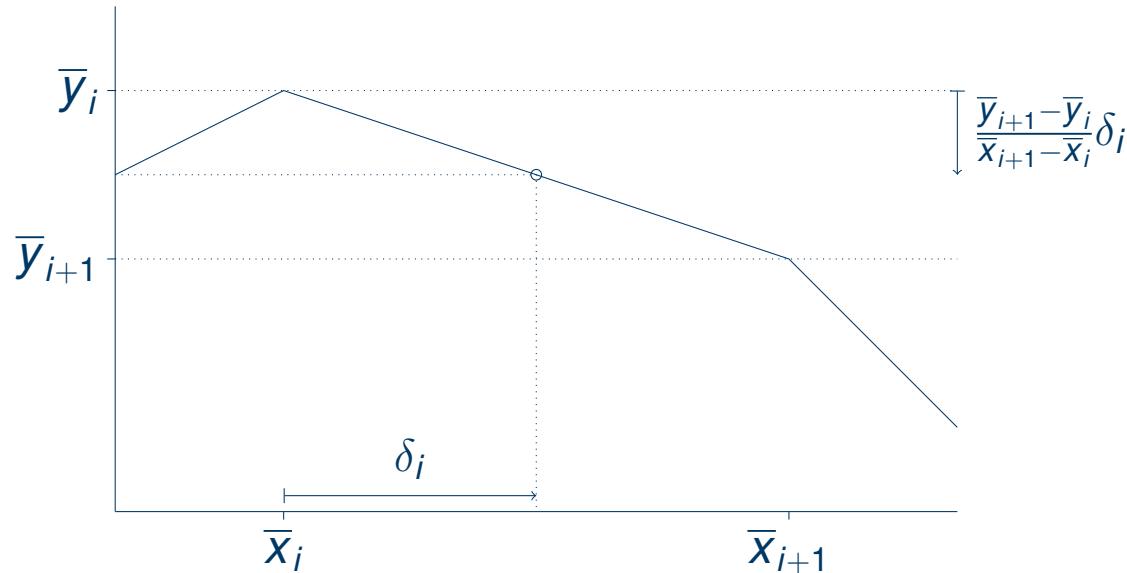
## MIP relaxations



- uses MIP formulations to approximate nonlinear constraints, e.g. incremental method or convex combination method.
- modify classical formulations to incorporate over- and underestimators (Geißler, Martin, Morsi, LS; 2012)

# Incremental Method: Basics

Markowitz, Manne (1957)



$$x = \bar{x}_0 + \sum_{i=1}^n \delta_i \quad y = \bar{y}_0 + \sum_{i=1}^n \frac{\bar{y}_i - \bar{y}_{i-1}}{\bar{x}_i - \bar{x}_{i-1}} \delta_i$$

$$(\bar{x}_{i-1} - \bar{x}_{i-2}) z_{i-1} \leq \delta_i \quad \text{for all } i = 1, \dots, n., \\ \delta_i \leq (\bar{x}_i - \bar{x}_{i-1}) z_i \quad \text{for all } i = 1, \dots, n-1.$$

# Incremental method

Incorporating approximation errors (Geissler, Martin, Morsi, LS; 2012)

$$x = \bar{x}_0 + \sum_{i=1}^n \delta_i$$

$$y = \bar{y}_0 + \sum_{i=1}^n \frac{\bar{y}_i - \bar{y}_{i-1}}{\bar{x}_i - \bar{x}_{i-1}} \delta_i + e$$

$$\epsilon_u^1(f) + \sum_{i=1}^{n-1} z_i (\epsilon_u^{i+1}(f) - \epsilon_u^i(f)) \geq e$$

$$-\epsilon_o^1(f) - \sum_{i=1}^{n-1} z_i (\epsilon_o^{i+1}(f) - \epsilon_o^i(f)) \leq e$$

$$\begin{aligned} (\bar{x}_{i-1} - \bar{x}_{i-2}) z_{i-1} &\leq \delta_i \quad \text{for all } i = 1, \dots, n, \\ \delta_i &\leq (\bar{x}_i - \bar{x}_{i-1}) z_i \quad \text{for all } i = 1, \dots, n-1. \end{aligned}$$

# What can be computed now?

test set	$ V $	$ A_{pi} $	$ A_{sc} $	$ A_{va} $	$ A_{cv} $	$ A_{cg} $	# nom.
HN-AB	661	498	116	33	26	7	43
HN-SN	592	452	98	35	23	6	4227
gaslib-582	582	451	96	26	23	5	4227
gaslib-582-95	582	451	96	26	23	5	4227

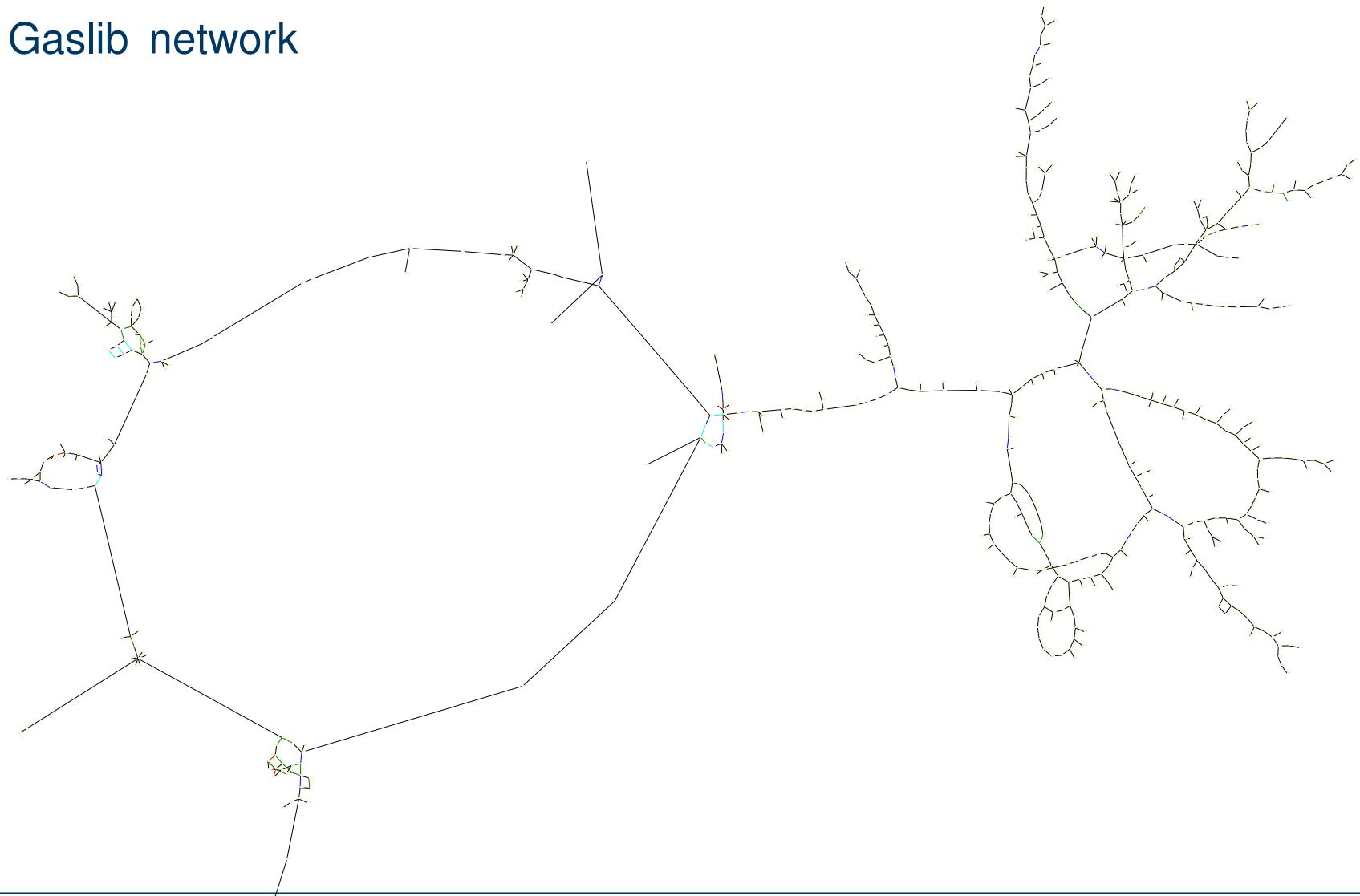
## Public instances

gaslib-582 and gaslib-582-95 are available at:

<http://gaslib.zib.de/>

# Impression

## Gaslib network

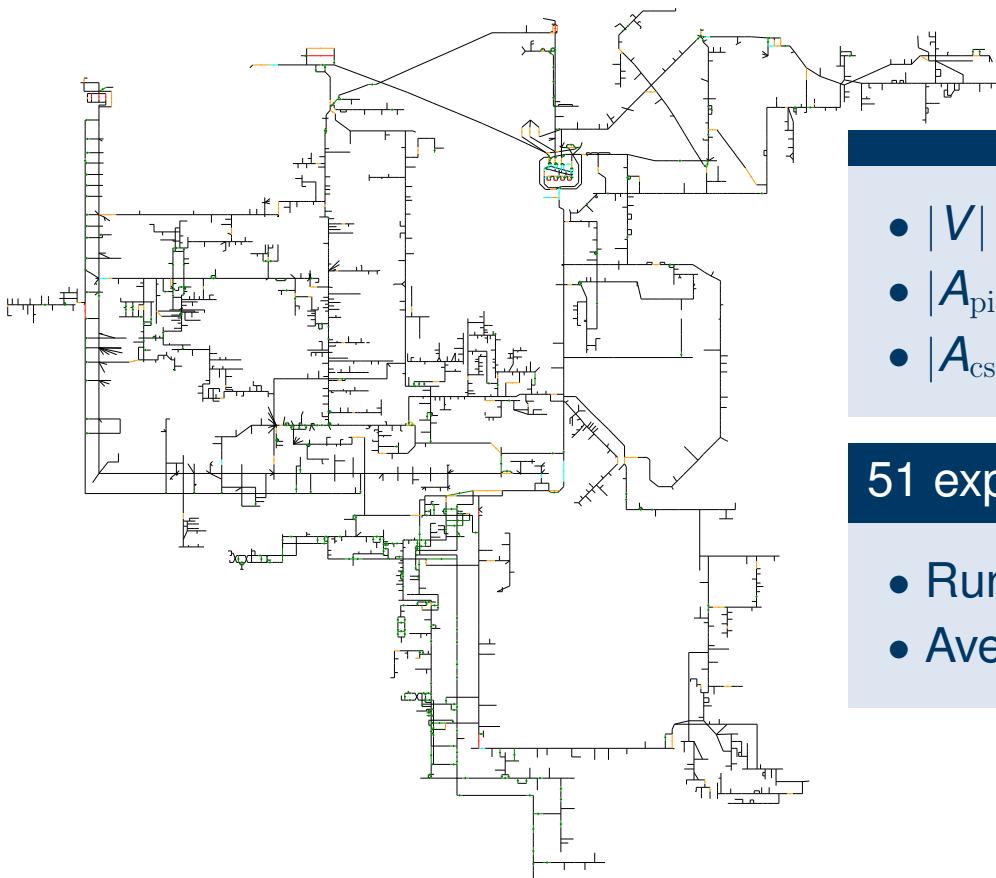


# Computational results – MILP approach

	slack 0	infeasible	slack > 0	no solution
HN-AB	33	3	7	0
HN-SN	3280	444	495	7
gaslib-582	2054	909	1230	34
gaslib-582-95	2831	716	661	19

- Timelimit: 14 400 s

# New variant of the MILP approach under development

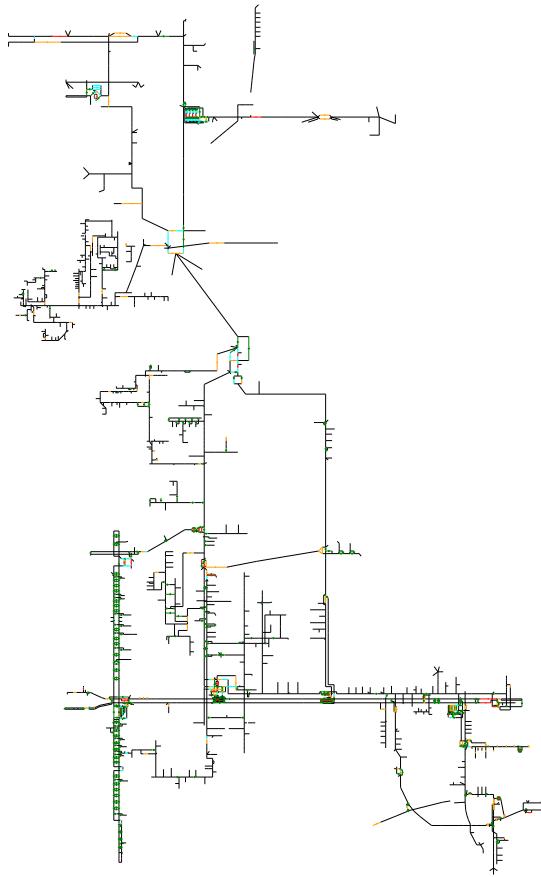


- $|V| = 4460,$
- $|A_{pi}| = 3550,$
- $|A_{cs}| = 12.$

51 expert instances

- Run time: 13 min to 810 min
- Average run time: 150 min

# New variant of the MILP approach under development



- $|V| = 2735,$
- $|A_{pi}| = 3074,$
- $|A_{cs}| = 41.$

29 expert instances

- Run time: 3 h to 49 h
- Average run time: 17 h

# Future directions

# Problems

## Standard contract

*“On any given day you are allowed to supply/demand up to  $X$  units of gas at node  $v$  if you have matching partners at some other nodes”*

## Problems

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# There is much to do

## Better physics

- Transient, non-isothermal,
- Gas mixtures,
- reach “simulation accuracy”.

## More economy

- Booking validation,
- Technical capacities,
- Network extension planning.

## Overall

- Faster,
- larger networks.

# Next up . . .

DFG CRC/TR 154

Mathematical modelling, simulation and optimization using the example of gas networks

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