



Simple maths for complex flows

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Farkas Miklós Seminar on Applied Analysis, BME

23 November 2023



- Hardcore (HC) fluid mechanics: an introduction
- Three representative practical case studies, with various working fluids
 - Water mill in the Danube: **water**
 - Clean room: **air**
 - Dryer: mixture of **hot flue gas + air**
- Summary: from a perspective of mathematics, in an evolutionary approach
- An interactive seminar
- Please feel free to put questions and give comments intermediately (sufficient timeframe)
- Interactions: questions and answers, discussion
-  **„Organized interaction“: + Interactions**
26 questions
- → Premium scores for you
- → You will be declared as a titular HC fluids engineer
- → Valuable prizes



HARDCORE FLUID MECHANICS



What does „hardcore” mean ?

HARDCORE

In music: „HC is generally faster, thicker, and heavier than earlier punk rock.” (*Wikipedia*)

HARDCORE FLUID MECHANICS

BME Department of Fluid Mechanics:

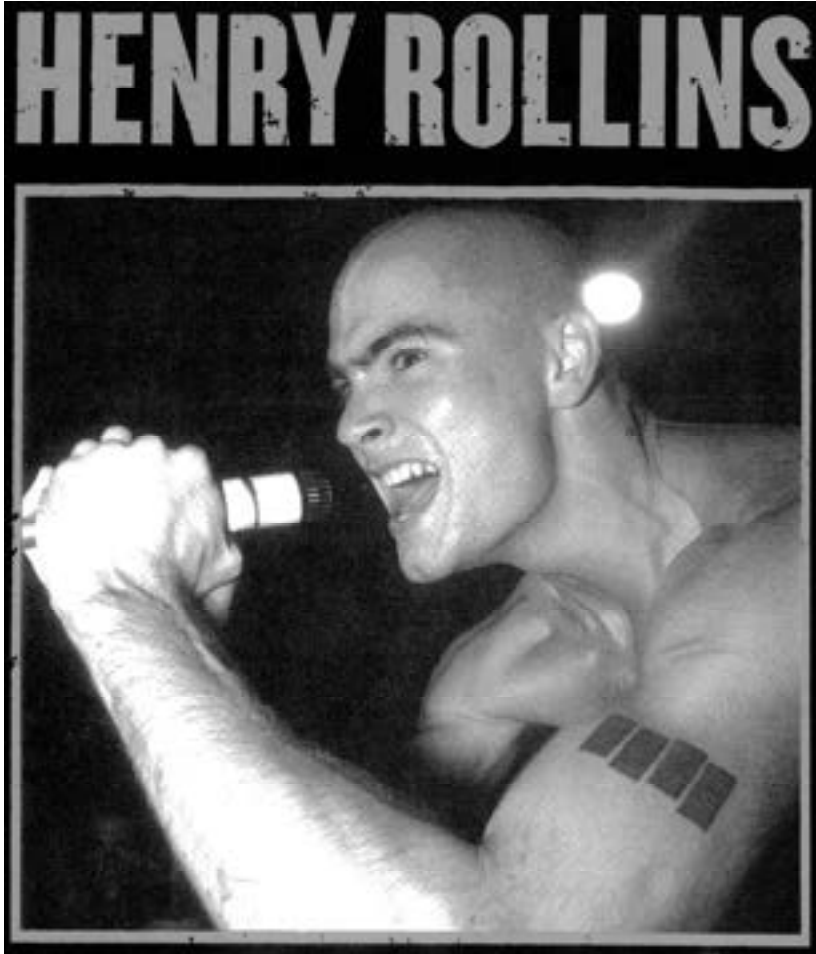
a „hardcore” group of fluids engineering scene

- Committed to engineering applications
- Firm in solving practical problems
- No hesitation – making decisions, often rapidly

→ **Relevant, brief, quick practical approximations**



- [For refinements of engineering calculations, validated by detailed experiments: advanced physics + mathematics: analysis; Computational Fluid Dynamics (CFD), ...]
- Basic physics and maths: primary-school-level → middle-school-level → ...
- Minimal modelling: *Einstein*: „A model should be as simple as it can be but no simpler”
- Aims:
 - Quick and brief (order-of-magnitude) estimations (even enabling mental arithmetic)
 - Confirmation ↔ rebuttal of feasibility of operational / constructional concepts
 - Preliminary design of parameters
 - Preliminary design of distributions
 - ... and more
- „Keep it simple”: old-school methods and tools
 - Available in the past centuries!
 - Available almost everywhere for you, being at your hand – even in a desert island!
- WHAT TOOLS?



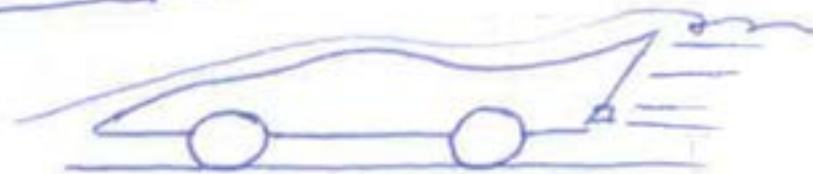
„Keep
•your blood clean,
•your body lean,
•and your mind sharp.”

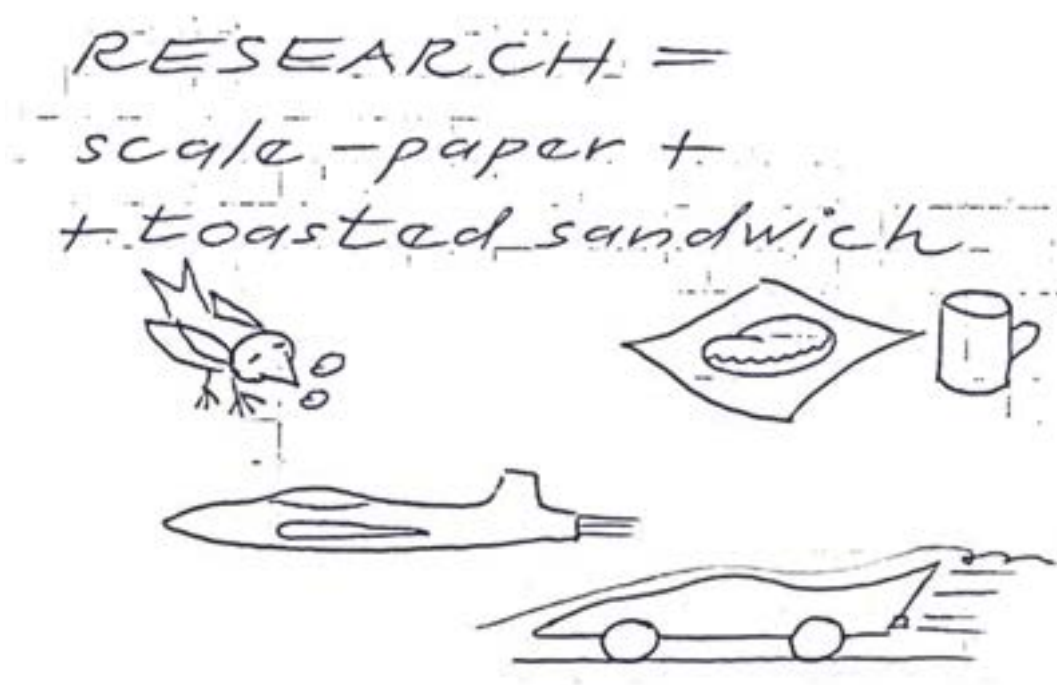
- Use your brain
- Be brave (to make sketches etc.)
- Be critical / self-critical



Break – ?

RESEARCH =
scale - paper +
+ toasted sandwich – Dr. Gergely KRISTÓF





+ a pen / pencil



- Three case studies
 - Engineering relevance, AND
 - Strengthening your social relations by means of FLUID MECHANICS:
 - How making new friends / a girlfriend / a boyfriend?
 - How promoting your mobile phone communication?
 - How contributing to the morning cornflakes of your family?
- FLUID MECHANICS: no „mistification”, no „rocket science” (at least in these examples): real life, „everyday miracles”
- FLUID MECHANICS: sexy, cool, trendy
- An intellectual pleasure, an exciting game – ENJOY!



II. CASE STUDY 1: WATER MILL IN THE DANUBE

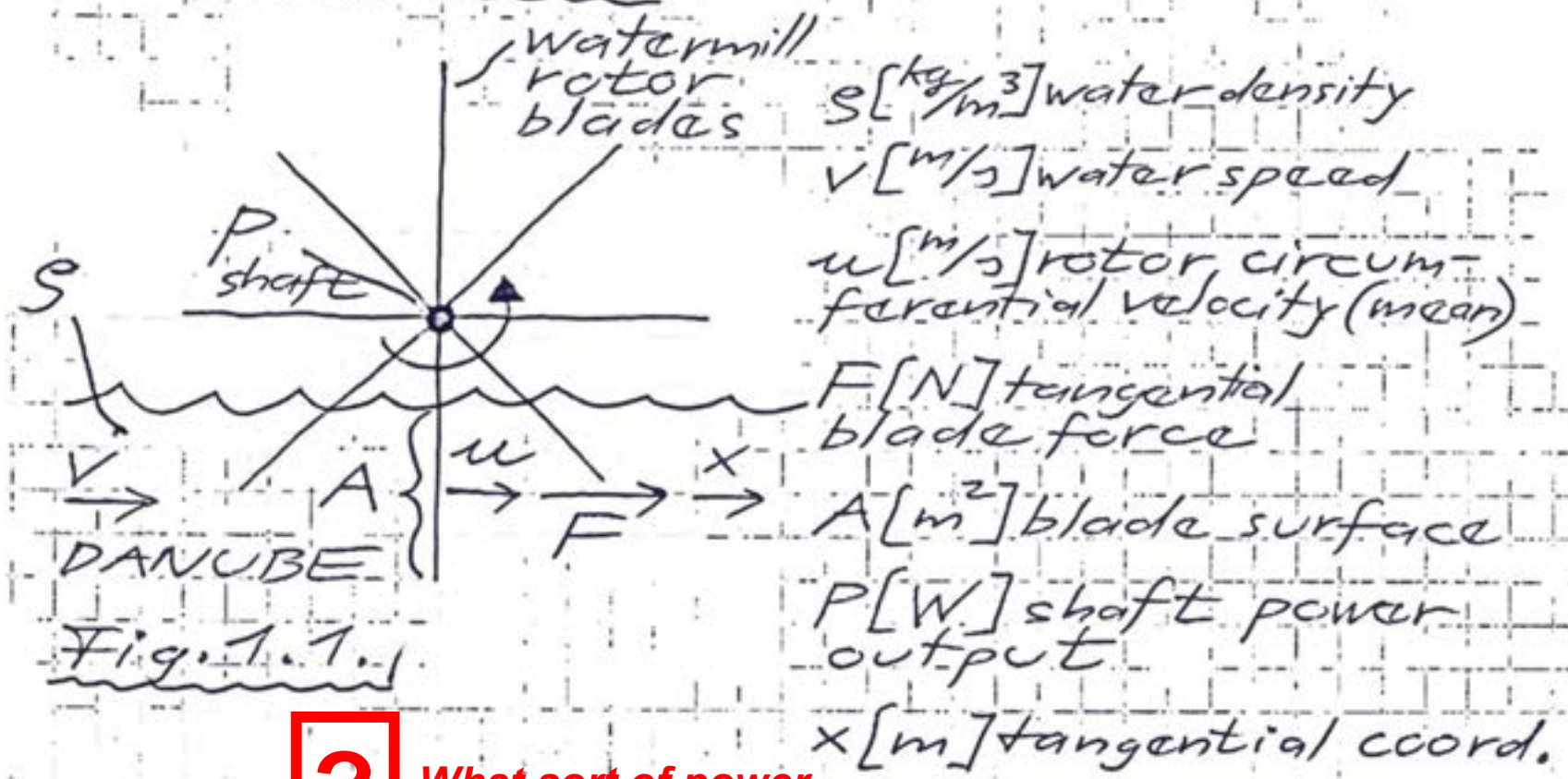
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- The story started at a party on a New Years' Day: eating, drinking, making music...
- Artists: painters, sculptors, photographers, a glass blower...
- + A single mechanical engineer (in fluid mechanics)
- Artistic inspirations: flying birds, waving water, blazing flames, billowing clouds...
- The idea by the glass blower:
 - A water mill on a boat in the Danube
 - Generating electricity for an electric glass smelter furnace
 - Glass blowing as tourist attraction + onboard restaurant for tourists...
- Is the idea technically feasible?
- Only some minutes are available for the answer → then losing the artists' interest
- Tools: a piece of paper napkin, + a pen
- Very brief outline of the following description on the paper napkin

II. CASE STUDY 1: WATER MILL IN THE DANUBE

1.1) Sketch:

A practical illustration is always beneficial

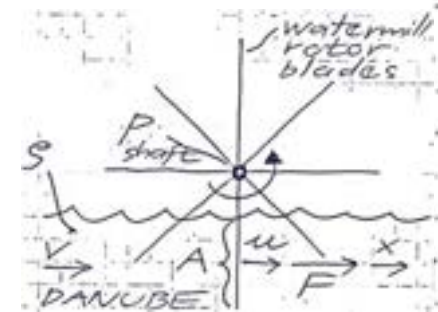


- ρ [kg/m³] water density
- v [m/s] water speed
- w [m/s] rotor circumferential velocity (mean)
- F [N] tangential blade force
- A [m²] blade surface
- P [W] shaft power output
- x [m] tangential coord.



What sort of power is the final aim ?

II. CASE STUDY 1: WATER MILL IN THE DANUBE



1.2) Formulation of problem:

P prescribed (demanded) \leftarrow

a) How to set " u " for maximum obtainable power P_{max} ? \leftarrow operational demand

b) $A = ?$ \leftarrow geometrical (design) demand

1.3) Assumptions:

"Idealistic" scenario: all losses neglected; maximum utilization of blades (no blade interference etc.)

$$P = P_{id} \leftarrow u; A_{\min} \quad (1.1)$$

minimum necessary

? $F; u \rightarrow P?$

? Examples for loss sources?

1.4) Solution / description:

1.4) Solution / description:

$$P = F \cdot u \quad [W] = \left[\frac{J}{s} \right] = \left[\frac{N \cdot m}{s} \right] \quad (1.2)$$

$F = ? \leftarrow$ Newton II.



$F \sim$ temporal rate of change of what?

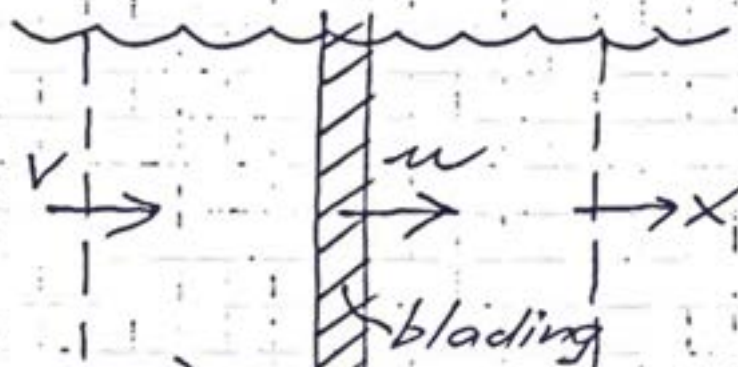


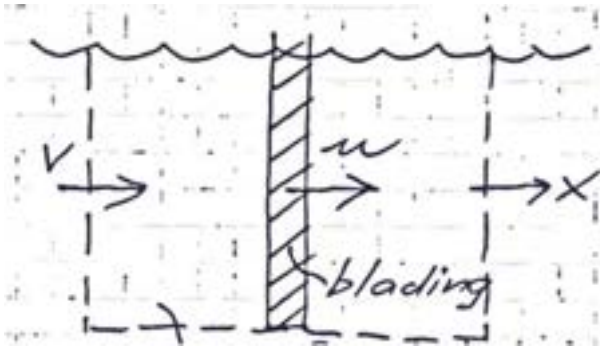
Fig. 1.2.



Mass; velocity \rightarrow momentum?

$\Delta m [kg]$: inlet water mass in duration of $\Delta t [s]$

II. CASE STUDY 1: WATER MILL IN THE DANUBE



x-wise (tangential) inlet momentum:

$$\Delta I_{in} = \Delta m \cdot v \quad (1.3)$$

$[kg] \cdot [m/s]$

Inlet x-wise momentum flux:

$$\frac{\Delta I_{in}}{\Delta t} \hat{=} \dot{I}_{in} = \frac{\Delta m}{\Delta t} \cdot v \quad (1.4)$$

$[kg/s] \cdot [m/s] = [kg \cdot \frac{m}{s^2}]$

Where

$$\frac{\Delta m}{\Delta t} \hat{=} \dot{q}_m \text{ mass flow rate } [\frac{kg}{s}] \quad (1.5)$$

$$\dot{q}_m [kg/s] = \rho \cdot v \cdot A \quad (1.6)$$

$[\frac{kg}{m^3}] \cdot [\frac{m}{s}] \cdot [m^2] = [\frac{kg}{s}]$

$$v \cdot A \hat{=} \dot{q}_v \text{ volume flow rate } (1.7)$$

$[\frac{m}{s}] \cdot [m^2] = [\frac{m^3}{s}]$

(1.4):

$$\text{momentum flux} = \text{mass flow rate} \times \text{velocity} \quad (1.8)$$



ρ for water ?

II. CASE STUDY 1: WATER MILL IN THE DANUBE

$$\dot{I}_{in} = \rho_m \cdot v = (\rho \cdot v \cdot A) \cdot v \quad (1.9)$$

Outlet momentum flux:

$$\dot{I}_{out} = \rho_m \cdot u = (\rho \cdot v \cdot A) \cdot u \quad (1.10)$$

constrained by the blading

Newton II: $[N = \frac{kg \cdot m}{s^2}] = [\frac{kg}{s}] \cdot [\frac{m}{s}]$

$$\dot{I}_{in} - \dot{I}_{out} = F = (\rho \cdot v \cdot A) \cdot \underbrace{(v - u)}_{\text{deceleration}} \quad (1.11)$$

(1.2)(1.11) \rightarrow

$$P = (\rho \cdot v \cdot A) \cdot (v - u) \cdot u \quad (1.12)$$

a) How to set "u" for maximum P?

- If $u = 0$: $F = F_{max}$ but $P = F \cdot u = 0$ (1.13a)

- If $u = v$: (free running):
 $u = u_{max}$ but $F = 0 \rightarrow P = 0$ (1.13b)

$u = ?$ - A quick, intuitive choice
 "in between"



What is your hint for u ?



How to determine u theoretically ?

$$u := \frac{v}{2} \quad (1.14)$$

Justification: (1.12) \rightarrow

$$\frac{\partial P}{\partial u} = (S \cdot v \cdot A) \cdot \frac{\partial [(v-u) \cdot u]}{\partial u} \stackrel{!}{=} 0 \quad (1.15a)$$

$$\begin{aligned} (-1) \cdot u + (v-u) &= 0 \\ v - 2u &= 0 \\ \underline{u} &= \underline{2u} \quad \checkmark \end{aligned}$$

$$\frac{\partial^2 P}{\partial u^2} : \frac{\partial}{\partial u} (v - 2u) = \underline{-2} < 0 \quad \checkmark \quad (1.15b)$$

maximum! \checkmark (1.15c)

b) $A_{min} = ?$

(1.12)(1.14) \rightarrow

$$P_{maxid} = (S \cdot v \cdot A_{min}) \cdot \left(v - \frac{v}{2}\right) \cdot \frac{v}{2} =$$

$$= S \cdot v^3 \cdot A_{min} \cdot \frac{1}{4} \quad (1.16a)$$

$$A_{min} = \frac{4 \cdot P_{maxid}}{S \cdot v^3} \quad (1.16b)$$



v for the Danube ? – Estimate: let's walk



Area for the classroom ? – Estimate

$$A_{min} = \frac{4 \cdot P_{maxid}}{\rho \cdot v^3} \quad (1.16b)$$

1.5) Calculation example:

choice of input data:

$$\rho = 10^3 \text{ kg/m}^3$$

$$v = 1 \text{ m/s}$$

$P_{maxid} = ?$ Household electric oven: 5 kW → small glass smelter furnace: $\approx 20 \text{ kW} = 2 \cdot 10^4 \text{ W}$

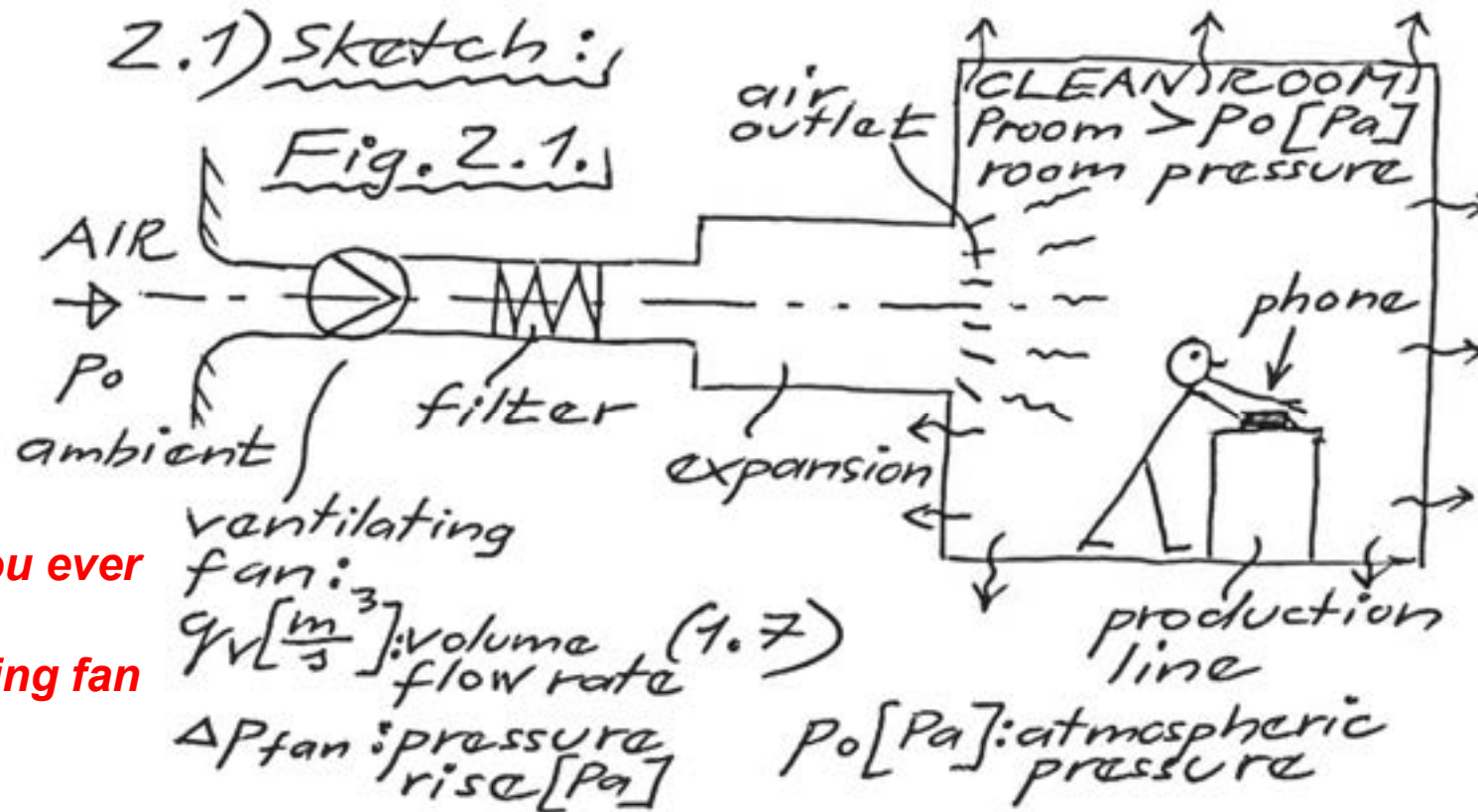
$$A_{min} = \frac{4 \cdot 2 \cdot 10^4}{10^3 \cdot 1^3} = 80 \text{ m}^2$$

Unfeasibly large surface (even for idealistic circumstances) → unrealistic to realize (technical + legislation issues...)

Issue with v on the cube in the denominator! ← Water turbine technology: for rushing rivers; for advanced water turbines with a dam

Impact on girls and boys at the party

Hardcore fluid mechanics: an effective tool for making new friends / a girlfriend / a boyfriend



? Have you ever seen a ventilating fan?

A practical illustration is always beneficial

? p_0 estimate?

Δp_{fan} pressure rise:

- o Covering flow friction losses
- o Maintaining room overpressure ($p_{room} - p_0$)
 - ~ against the infiltration of contaminated (dusty) ambient air:
 - ~ only outward flow is allowed, via air gaps etc. (no inward flow of unfiltered air!)

2.2) Assumptions

"Small" changes in pressure and temperature $\rightarrow \rho = \text{constant}$ air density
 [kg/m³]: incompressible approach

2.3) Sudden duct expansion

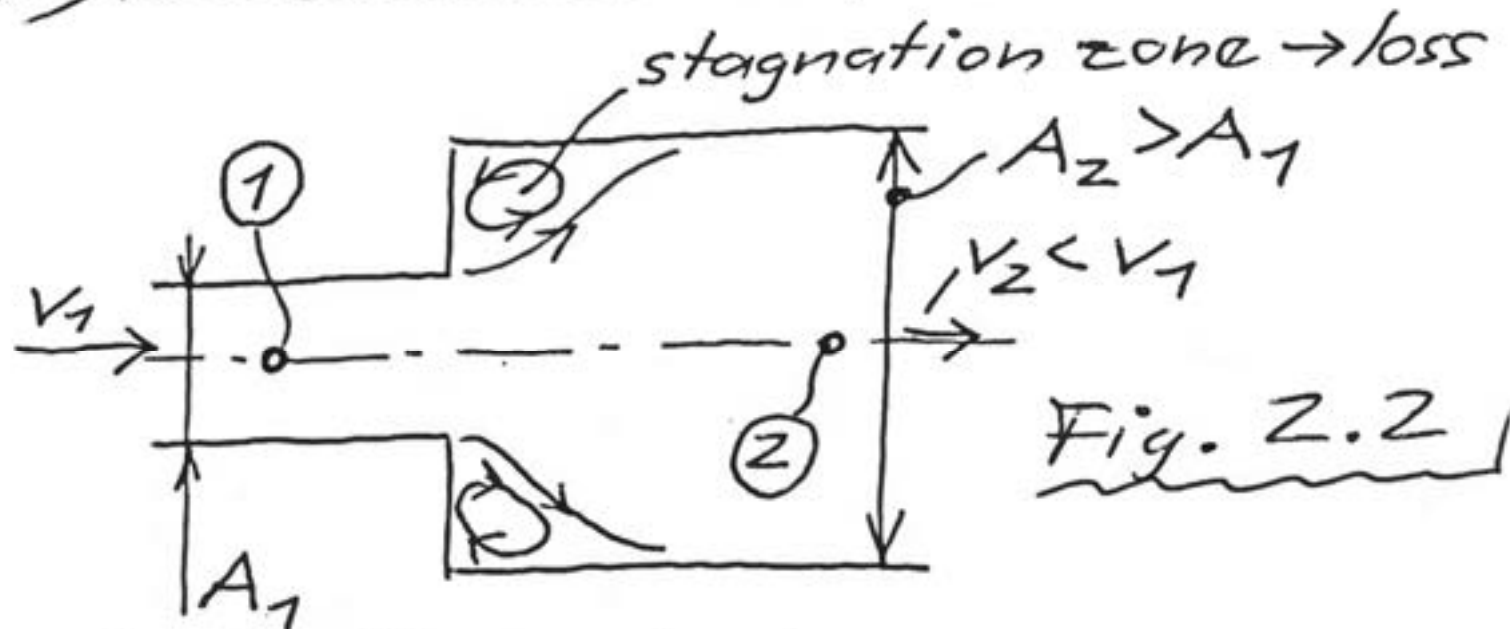
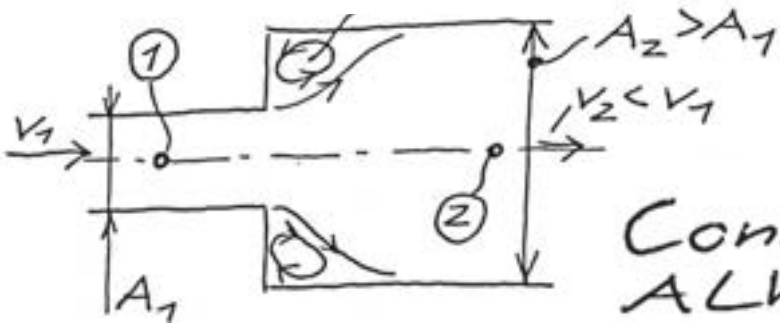


Fig. 2.2

$v [m/s] \sim$ flow velocity
 $A [m^2] \sim$ cross-sectional area



Why sudden ?
 What can we spare ? What is cheaper ?



Conservation of fluid mass:
 ALWAYS valid in classic mechanics:
 Mass flow rate: (1.6)

$$\dot{q}_{m1} = \dot{q}_{m2} \text{ [kg/s]} \quad (2.1a)$$

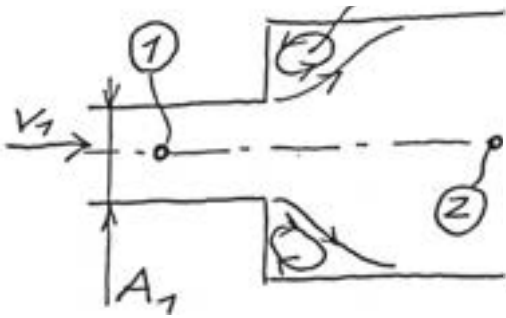
$$\rho v_1 A_1 = \rho v_2 A_2 \quad (2.1b)$$

$$v_1 A_1 = v_2 A_2 \quad (2.1c)$$

$$\dot{q}_{v1} = \dot{q}_{v2} \text{ [m}^3\text{/s]} \quad (2.1d)$$

Volume flow rate (1.7)

v_1, A_1 : tailored by the fan (given)



Conservation of energy:
 Bernoulli equation $1 \rightarrow 2$:

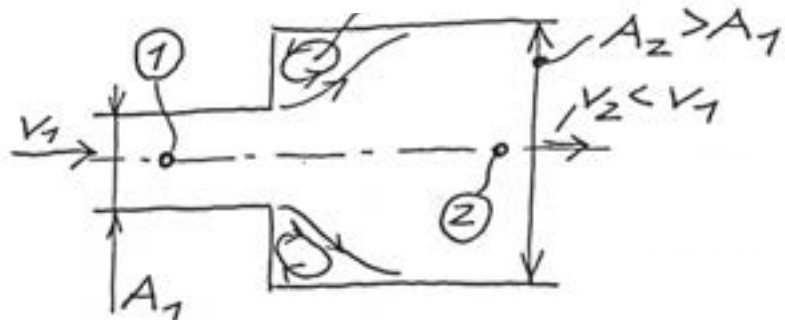
$$p_1 + \rho \frac{v_1^2}{2} = p_2 + \rho \frac{v_2^2}{2} + \Delta p' \quad (2.2a)$$
 static pressure dynamic pressure pressure loss
 (\leftarrow kinetic energy) (\leftarrow flow friction)

$$\left[\frac{v^2}{2} \right] = \frac{J}{kg}$$

$$\left[\rho \frac{v^2}{2} \right] = \frac{J}{kg} \cdot \frac{kg}{m^3} = \frac{J}{m^3}$$

$$p_2 - p_1 \stackrel{\Delta p}{=} = \rho \left(\frac{v_1^2}{2} - \frac{v_2^2}{2} \right) - \Delta p' \quad (2.2b)$$

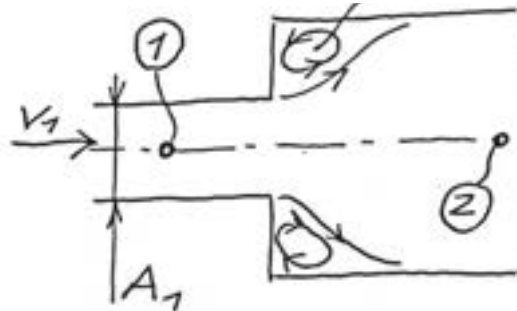
pressure recovery



An example: lower velocity \rightarrow
lower loss \rightarrow less cost ?

Benefits of expansion:

- o $v_2 < v_1$ slower outflow;
no draft \rightarrow good for human health
- o less velocity: $v_2 < v_1 \rightarrow$ moderate
flow friction loss (energetically
more favourable)
- o $v_2 < v_1 : p_2 > p_1$: pressure recovery
 Δp : contributes to $p_{room} > p_o$



Pressure recovery coefficient:

$$C_p = \frac{P_2 - P_1}{\rho \frac{v_1^2}{2}} = \frac{\Delta P}{\underbrace{\rho \frac{v_1^2}{2}}_{\text{inlet specific kinetic energy}}} \quad (2.3)$$

"Pressure increasing capability per unit inlet kinetic energy"

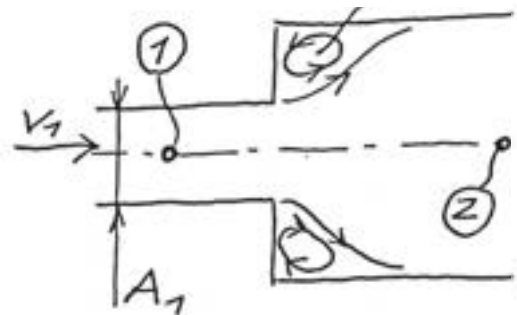
Area ratio: $n_{AR} = \frac{A_2}{A_1} \quad (2.4)$

(2.1c) \rightarrow

$$n_{AR} = \frac{v_1}{v_2} \quad (2.4a)$$

2.4.) Formulation of problem

How to select n_{AR} to obtain maximum C_p ? "Energetically efficient behaviour"



2.5.) Solution / description

→ The more the nAR → the more the deceleration ($v_2 < v_1$) → the more the potential for pressure recovery due to reducing the dynamic pressure:

"ideal pressure rise: $\rho \left(\frac{v_1^2}{2} - \frac{v_2^2}{2} \right)$ "

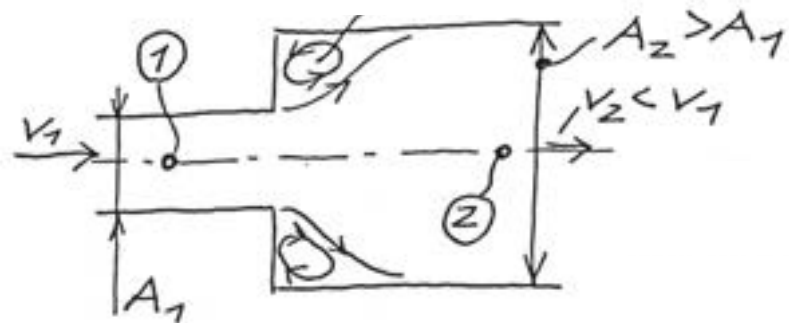
→ The less the nAR → the less drastic change in flow path → reduced stagnation zone → moderation in $\Delta p'$ deteriorating the pressure recovery



Any ideas ?

How to find an intermediate compromise in nAR for maximum Cp ? $\Delta p = \rho \left(\frac{v_1^2}{2} - \frac{v_2^2}{2} \right) - \Delta p'$ (2.2b)

III. CASE STUDY 2: CLEAN ROOM FOR MOBILE PHONE PRODUCTION



How to find an n_{AR}
to maximize C_p ?

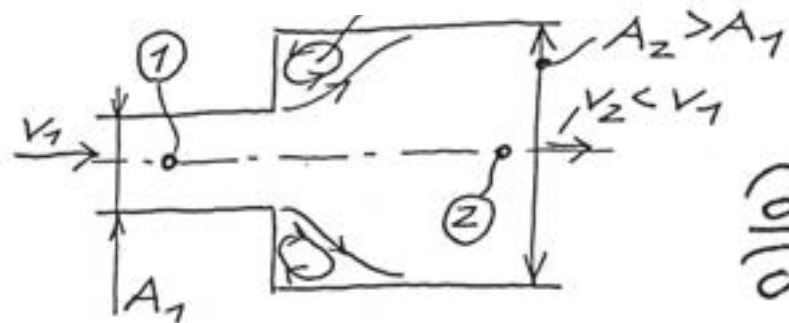
"Borda - Carnot equation"
"Sudden expansion of a pipe"
(Internet, e.g. Wikipedia)

$$\Delta p' = \frac{\rho}{2}(v_1 - v_2)^2 \quad (2.5)$$

$$\begin{aligned} (2.2b)(2.5) &\rightarrow \\ \Delta p &= \underbrace{\rho \left(\frac{v_2^2}{2} - \frac{v_1^2}{2} \right)}_{\text{ideal pressure rise}} - \underbrace{\frac{\rho}{2}(v_1 - v_2)^2}_{\Delta p'} = \\ &= \frac{\rho}{2} \{ v_2^2 - v_1^2 - (v_1 - v_2)^2 \} = \\ &= \frac{\rho}{2} \{ (v_1 + v_2)(v_1 - v_2) - (v_1 - v_2)(v_1 - v_2) \} = \\ &= \frac{\rho}{2} (v_1 - v_2) \{ (v_1 + v_2) - (v_1 - v_2) \} = \\ &= \frac{\rho}{2} (v_1 - v_2) \cdot 2v_2 = \Delta p \quad (2.6) \end{aligned}$$

$$\begin{aligned} C_p &= \frac{\Delta p}{\rho \frac{v_1^2}{2}} = \frac{\frac{\rho}{2} (v_1 - v_2) \cdot 2v_2}{\rho \frac{v_1^2}{2}} = \\ &= 2 \cdot \left[1 - \frac{v_2}{v_1} \right] \cdot \frac{v_2}{v_1} = C_p \quad (2.7) \end{aligned}$$

$$(2.7)(2.4a) \rightarrow C_p = 2 \cdot \left[1 - \frac{1}{n_{AR}} \right] \cdot \frac{1}{n_{AR}} \quad (2.8)$$



$$\begin{aligned} \frac{\partial C_p}{\partial n_{AR}} &= Z \cdot \left\{ \left[\frac{1}{n_{AR}^2} \cdot \frac{1}{n_{AR}} \right] + \left[1 - \frac{1}{n_{AR}} \right] \cdot \frac{(-1)}{n_{AR}^2} \right\} = \\ &= Z \cdot \left\{ \frac{1}{n_{AR}^3} - \frac{1}{n_{AR}^2} + \frac{1}{n_{AR}^3} \right\} = \\ &= Z \cdot \left\{ \frac{2}{n_{AR}^3} - \frac{1}{n_{AR}^2} \right\} = \frac{Z}{n_{AR}^2} \left\{ \frac{2}{n_{AR}} - 1 \right\} \end{aligned} \quad (2.9)$$

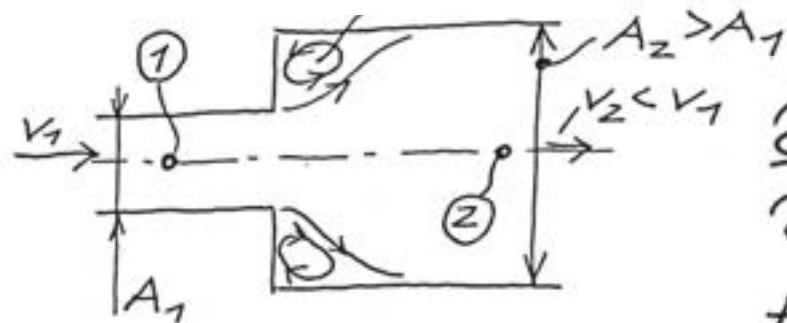
$$\frac{\partial C_p}{\partial n_{AR}} := 0 ; \quad \frac{Z}{n_{AR}} = 1 \quad (2.10)$$

$n_{AR} = Z$



What is missing ?

III. CASE STUDY 2: CLEAN ROOM FOR MOBILE PHONE PRODUCTION



$$\frac{\partial^2 C_p}{\partial n_{AR}^2} = + \frac{Z \cdot (-2)}{n_{AR}^3} \left\{ \frac{Z}{n_{AR}} - 1 \right\} + \frac{Z}{n_{AR}} \left\{ -\frac{Z}{n_{AR}} \right\} \quad (2.11a)$$

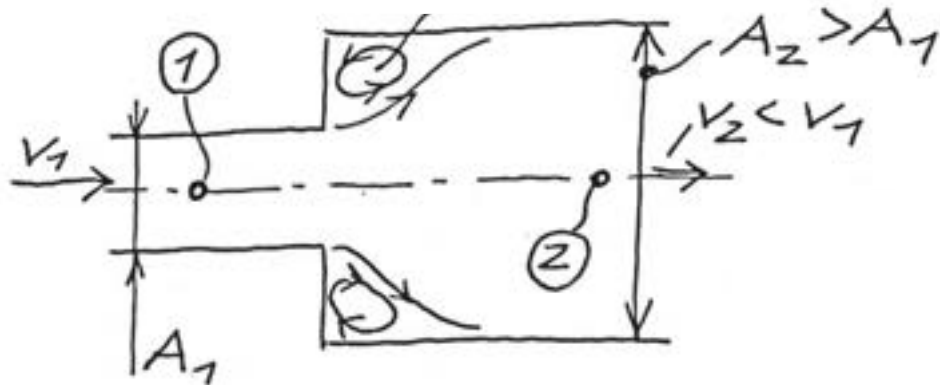
$$\text{@ } n_{AR} = Z: \\ -\frac{4}{Z^3} \left\{ \frac{Z}{Z} - 1 \right\} + \frac{Z}{Z^2} \left\{ -\frac{Z}{Z^2} \right\}$$

$$\frac{\partial^2 C_p}{\partial n_{AR}^2} \Big|_{\text{maximum}} \Big|_{n_{AR}=Z} < 0 \quad \checkmark \quad (2.11b)$$

? Any issues with notation $\partial / \partial \dots$?

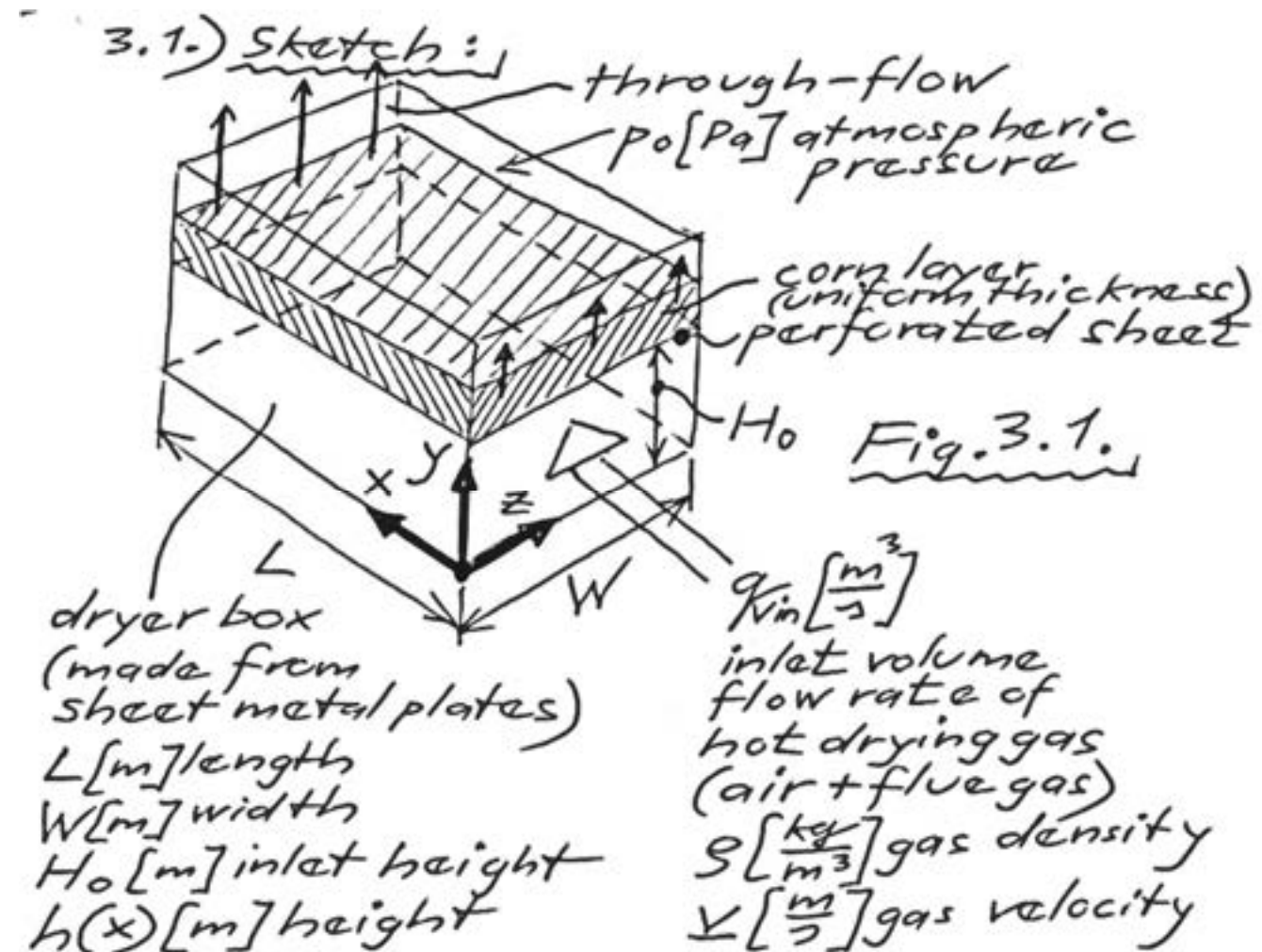
$n_{AR} = 2$ for $C_p \text{ max} = 0,5$

? Any historical example for a similar practical analytical solution of such complexity ?



- $n_{AR} = A_2 / A_1 = 2$ for the maximum of specific pressure recovery, resulting in $C_p = 0,5$
- The half of inlet dynamic pressure (\sim inlet kinetic energy) is converted to pressure rise
- Truly analytical solution, confirmed by experimental data (own and literature measurements)
- Sudden pipe expansions have been existing for centuries.
- Mathematical analysis has been existing for centuries.
- We have published this analytical solution first, in 2023!!! (*Lukács and Vad, 2023*)
- <https://pp.bme.hu/me/article/view/22389/9863> – Publication of detailed interpretation is in progress
- The World is small.

IV. CASE STUDY 3: CORN DRYER



?

What machinery delivers the gas ?

?

Combustion of what fuel, to obtain a „healthy” flue gas ?

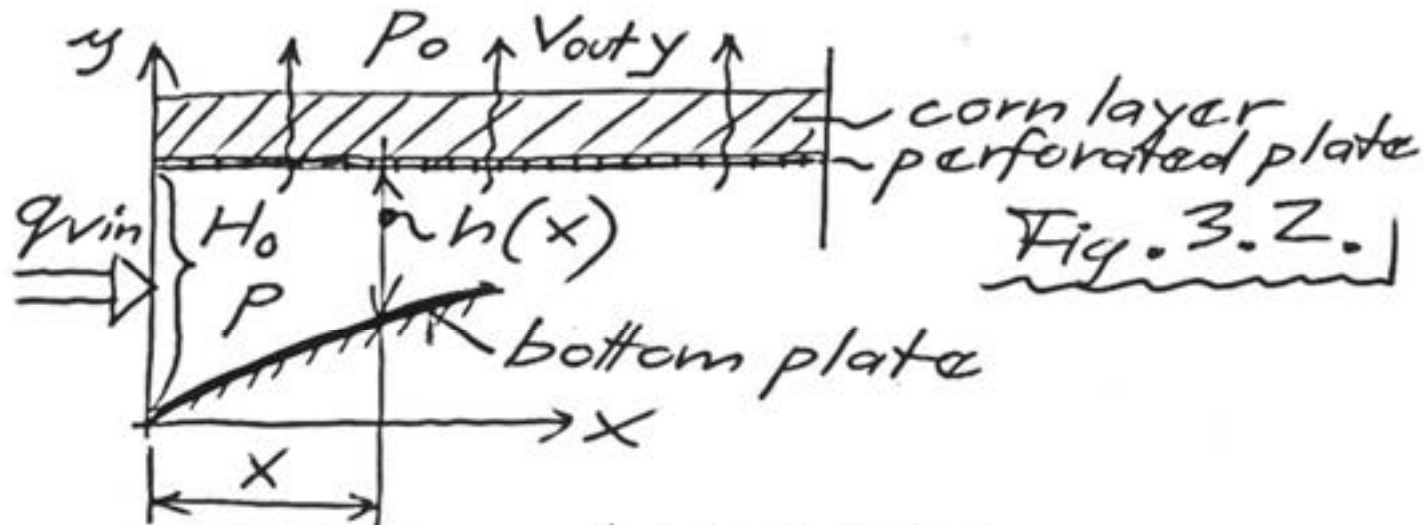
If the shape of the drying box is a rectangular cuboid:

3.2. Formulation of problem:
 $h(x) = \text{constant} \equiv H_0$ (3.1)
 IS BAD! non-uniform drying!
 y-wise outflow through the corn layer:
 - Near $x = 0$: "not enough"
 "underdrying"
 - Near $x = L$: "too much"
 "overdrying"
 → corn burn-out

How to set the longitudinal (x-wise) distribution of $h(x)$ for constant (uniform) y-wise through-flow?

3.3. Assumptions:
 i) $\rho = \text{constant}$ (incompressible) (3.2a)
 ii) $v_z \equiv 0$
 iii) $\partial/\partial z \equiv 0$
 iv) Wall flow friction neglected
 } 2D (planar) flow (3.2b, 3.2c)

3.4.) Solution / description:



p [Pa]: internal pressure
 v_{outy} [$\frac{m}{s}$]: outflow velocity
 $p - p_0 \stackrel{\Delta}{=} \Delta p$ [Pa] overpressure (3.3)

[Analogy with electricity:
Ohm's Law:

$$I = \frac{1}{R} \cdot \Delta U \quad (3.4a)$$

↑ current [C/s = A] resistance (permeability) CONSTANT voltage difference [V]

$$I \sim \Delta U \quad (3.4b)$$

$$V_{out} \sim \Delta p \quad (3.4c)$$

Uniform through-flow:

$v_{out y} \equiv \text{constant} \rightarrow (3.5a)(1.7): (3.5a)$

$v_{out y} = \frac{q_{vin}}{A_{layer}} = \frac{q_{vin}}{L \cdot W} \quad (3.5b)$

$(3.4c) \rightarrow$

$\Delta p(x) \equiv \text{constant} \quad (3.5c)$

$p(x) \equiv \text{constant} \quad (3.5d)$

How to obtain? $h(x) = ?$ $(3.5e)$

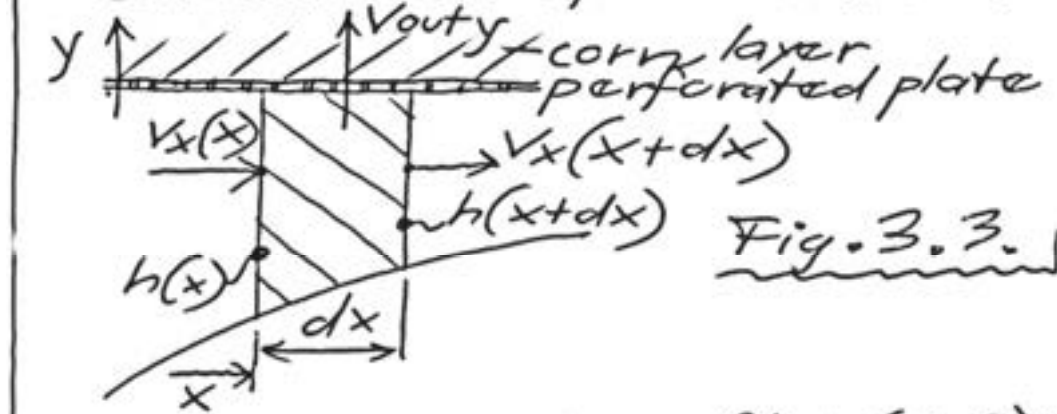
$\rightarrow p(x) \equiv \text{constant}: \text{NO } x\text{-wise aerodynamic force is generated}$



What principle (law) will be used?

Newton II:

NO x-wise aerodynamic force:
 (NO x-wise change in fluid momentum should be generated!)
 "Conservation of momentum"



x-wise momentum flux (1.8):

$$\dot{I}_x = \dot{q}_{mx} \cdot v_x = \underbrace{\left\{ \underbrace{\rho \cdot [h(x) \cdot W]}_A \cdot v_x \right\}}_{\text{const.}} \cdot v_x = \underbrace{\rho \cdot W \cdot h(x)}_{\dot{q}_m(x)} \cdot v_x^2 \quad (3.6a)$$

$\therefore = \text{constant!}$



What additional principle (law) is ALWAYS available?
 Conservation of...

$$\frac{dI_x}{dx} := 0 \quad (3.6a) \rightarrow \quad (3.6b)$$

$$\frac{dh}{dx} \cdot v_x^2 + h \cdot 2v_x \cdot \frac{dv_x}{dx} = 0 \quad (3.6c)$$

Additional equation – ALWAYS!
Conservation of fluid mass:
x-wise volume flow rate:

$$q_{vx} = v_x \cdot \underbrace{h \cdot W}_A \quad (3.7a)$$

$$-dq_{vx} = v_{outy} \cdot \underbrace{dx \cdot W}_{dA_{layer}} \quad (3.7b)$$

$$-\frac{dq_{vx}}{dx} = v_{outy} \cdot W \quad (3.7c)$$

$$(3.7a)(3.7c) \rightarrow -W \left(\frac{dv_x}{dx} h + v_x \frac{dh}{dx} \right) = v_{outy} \cdot W \quad (3.7d)$$

$$(3.6c) \rightarrow \frac{dv_x}{dx} = -\frac{dh}{dx} \frac{v_x^2}{h \cdot 2v_x} = -\frac{1}{2h} \frac{dh}{dx} v_x \quad (3.7e)$$

$$(3.7d)(3.7e) \rightarrow -\left[-\frac{1}{2h} \frac{dh}{dx} v_x h + v_x \frac{dh}{dx}\right] = v_{outy} = -\frac{1}{2} \frac{dh}{dx} v_x = v_{outy} \quad (3.8)$$

But

$$q_{vx}(x) = v_x(x) \cdot \underbrace{h(x) \cdot W}_A = q_{vin} - v_{outy} \cdot x \cdot W \quad (3.9a)$$

$$(3.5b) \rightarrow v_x \cdot h \cdot W = q_{vin} - \underbrace{\frac{q_{vin}}{L \cdot W} \cdot x \cdot W}_{v_{outy}} = q_{vin} \left[1 - \frac{x}{L}\right] \quad (3.9b)$$

$$v_x = \frac{q_{vin}}{h \cdot W} \left[1 - \frac{x}{L}\right] \quad (3.9c)$$

$$(3.8)(3.9c)(3.5b) \rightarrow$$

$$-\frac{1}{2} \frac{dh}{dx} \frac{q_{v, \text{in}}}{h \cdot W} \left[1 - \frac{x}{L}\right] = \frac{q_{v, \text{in}}}{L \cdot W} \quad (3.10a)$$

Solution: independent from $q_{v, \text{in}}$
ROBUST!

$$-\frac{1}{2} \frac{1}{h} \frac{dh}{dx} \left[1 - \frac{x}{L}\right] = \frac{1}{L} \quad (3.10b)$$

$$\bar{X} \hat{=} \frac{x}{L} \quad (3.11a)$$

$$H \hat{=} \frac{h}{H_0} \quad (3.11b)$$

$$(3.10b)(3.11a)(3.11b) \rightarrow$$

$$-\frac{1}{2} \frac{1}{H} \frac{dH}{d\bar{X}} \left[1 - \bar{X}\right] = 1 \quad (3.12a)$$

$$-\frac{1}{Z} \frac{dH}{H} = \frac{dX}{1-X} \quad (3.12b)$$

$$\int_1^H \frac{dH}{H} = -2 \int_0^X \frac{dX}{1-X} \quad (3.12c)$$

$$\ln H = 2 \ln(1-X) \quad (3.12d)$$

/exp

$$\underline{H = (1-X)^2} \quad (3.13)$$

Tangents :

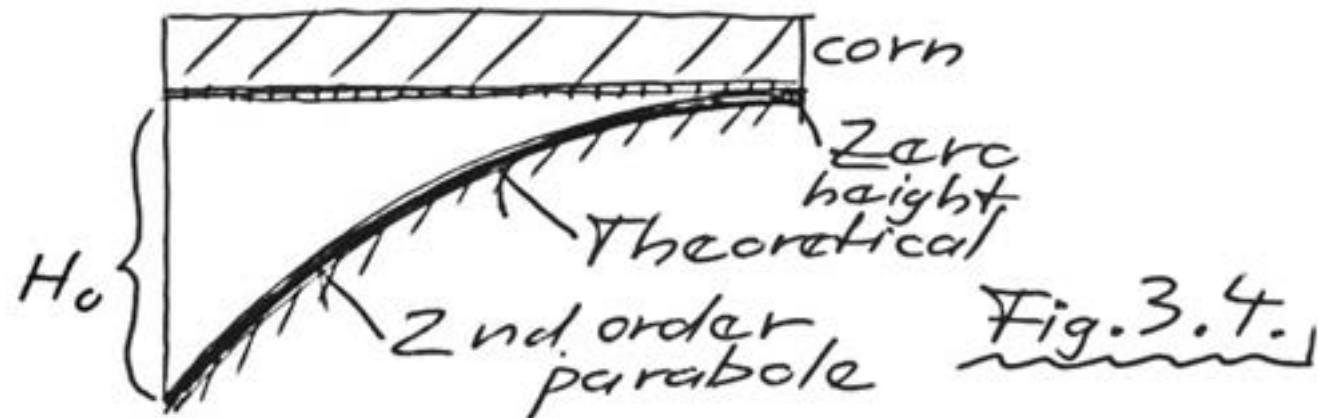
$$\frac{dH}{dX} = 2(1-X)(-1) \quad (3.14a)$$

$$@ X = 0 : \frac{dH}{dX} = -2 \quad (3.14b)$$

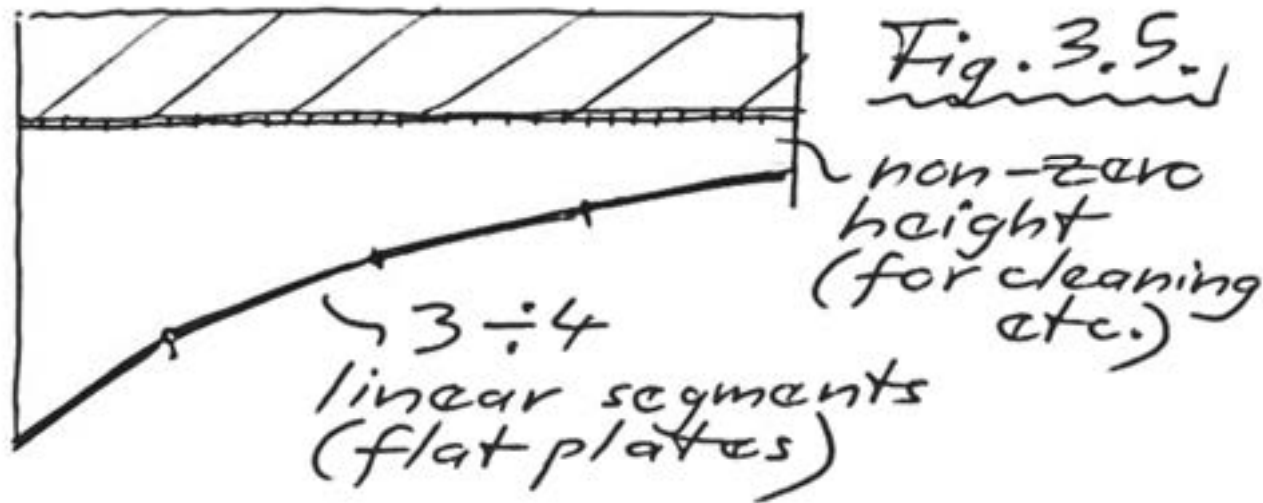
$$@ X = 1 : \frac{dH}{dX} = 0 \quad (3.14c)$$



What approximation would you recommend for easy and cost-effective manufacturing ?



3.5.)
Practical approximation:





Case study 1: Watermill in the Danube; turbine principle – WATER

- Complex 3D flow (← CFD...) in the vicinity of the rotor blades ← simplifications
- Order-of-magnitude estimations; confirmation / rebuttal of the feasibility of operational / design concepts
- **Mathematics tools: basic operations (multiplication, division, addition, extraction) → mental arithmetic; extreme analysis by means of derivation**

Case study 2: Clean room technology for mobile phone production – AIR

- Complex 3D flow in the stagnant zone (separation bubble) of the expansion ← simplifications
- Purposeful preliminary design of a parameter: area ratio for maximum pressure recovery
- **Mathematics tools: basic operations; extreme analysis by means of derivation**

Case study 3: Corn drying technology – HOT FLUE GAS + AIR MIXTURE

- Complex 3D flow in the vicinity of the corn gravels (within the layer) ← simplifications
- Purposeful preliminary design of a distribution: $h(x)$ for uniform through-flow
- **Mathematics tools: basic operations; derivation; ordinary differential equation; integration**



Simple maths for complex flows

THANK YOU FOR YOUR ATTENTION AND CONTRIBUTION!

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